

(19)



Europäisches Patentamt

European Patent Office

Office européen des brevets



(11)

EP 0 811 479 A2

(12)

## EUROPEAN PATENT APPLICATION

(43) Date of publication:

10.12.1997 Bulletin 1997/50

(51) Int Cl. 6: B32B 5/24, B32B 27/32,  
D04H 13/00, H01M 2/16

(21) Application number: 97303786.4

(22) Date of filing: 03.06.1997

(84) Designated Contracting States:

AT BE CH DE DK ES FI FR GB GR IE IT LI LU MC  
NL PT SE

Designated Extension States:

AL LT LV RO SI

(30) Priority: 04.06.1996 JP 163776/96

02.08.1996 JP 220465/96

(71) Applicant: Tonen Chemical Corporation  
Tokyo (JP)

(72) Inventors:

- Takita, Kotaro, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)

- Kono, Koichi, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)
- Kaimai, Norimitsu, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)
- Yamaguchi, Soichiro, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)

(74) Representative: Calamita, Roberto

Frank B. Dehn & Co.,  
European Patent Attorneys,  
179 Queen Victoria Street  
London EC4V 4EL (GB)

(54) **Microporous polyolefin composition membrane, production method thereof and battery separator**

(57) A microporous polyolefin composite membrane, preferably for use as a battery separator, comprising a microporous polyolefin membrane and a polyolefin nonwoven fabric laminated on at least one surface of the microporous polyolefin membrane. The composite membrane has a thickness of 25 to 200 µm, a porosity of 30 to 70%, an air permeability of 100 to 2000 sec/100cc and a surface opening area ratio of 50 to 90% on at least one outer surface thereof. The microporous polyolefin membrane comprises a matrix polyolefin component which is a polyolefin having a weight average molecular weight of  $5 \times 10^5$  or more or a polyolefin mixture containing the polyolefin having a weight aver-

age molecular weight of  $5 \times 10^5$  or more, and has a porosity of 30 to 95%, an air permeability of 100 to 2000 sec/100cc, an average open pore diameter of 0.001 to 1 µm and a tensile strength at break of 500 kg/cm<sup>2</sup> or more. The microporous polyolefin membrane may further comprise a shutdown polymer component to shut down the pores, thereby making the composite membrane impermeable. The polyolefin nonwoven fabric comprises fine fibers and has an air permeability of 0.1 to 100 sec/100cc and a basis weight of 5 to 50 g/m<sup>2</sup>. The polyolefin nonwoven fabric prevents the composite membrane from melting down at a low temperature thereby preventing the short-circuit between the electrodes.

**Description**

The present invention relates to a microporous polyolefin composite membrane for use as a separator of a non-aqueous battery such as a lithium battery. More specifically, it relates to a microporous polyolefin composite membrane which has an excellent permeability and mechanical strength as well as a high safety to shut down of permeability at a low temperature when an unusually large amount of heat is generated due to short circuit of the battery.

Microporous polyolefin membranes are widely used in various applications such as various filters, battery separators, electrolytic capacitor separators, etc. Since a lithium battery utilizes lithium metal and lithium ions, an aprotic organic polar solvent is used as the solvent for electrolyte such as a lithium salt. Therefore a microporous membrane or a nonwoven fabric, each made of a polyolefin such as polyethylene, polypropylene, etc. is used as the separator disposed between a negative electrode and a positive electrode, because they are insoluble in the aprotic organic polar solvent and chemically stable against the electrolyte and electrode active materials.

The lithium secondary battery is known as one of the secondary batteries of the highest energy density, because it has an electromotive force as high as 2.5 to 4 V and utilizes lithium having a low atomic weight as the main electrode active material. A button type or UM-3 type lithium secondary battery of a small capacity has been used as a backup battery for computer memory, a power source for handy phones, etc. However, since a capacity of about 10 kWh is required when a battery is applied to electric cars, etc., there has been a demand for the development of a lithium battery having an enhanced capacity and an enhanced output power. Since the aprotic organic polar solvent has a low electroconductivity, the electric current density of the lithium battery is low. Therefore, a large surface area of the electrodes is necessary to obtain a large-size lithium battery enhanced in both the capacity and output power.

The separator for use in such a battery is desired to have suitably small pores in its matrix. However, since the contact surface between the electrodes and the separator reduces the effective surface area of the electrodes, the separator is preferred to have a rough surface on the microscopic scale and a relatively large pore size on its surface. Also, the separator should have a reasonable thickness which keeps both the electrodes spaced from each other by a sufficient distance for safety. Further, the holding capacity of the separator for the electrolyte solution should be enhanced to assure good battery characteristics such as discharge property and cycle property.

Recently, there have been proposed various methods for producing a high-strength and high-modulus microporous membrane from an ultrahigh molecular weight (UHMW) polyolefin. For example, in one of the methods, a UHMW polyolefin composition is heated to an elevated temperature in a solvent to form a solution of UHMW polyolefin. This solution is extruded to form a gel sheet which is then stretched under heating and extracted to remove the solvent from the stretched sheet to form a microporous structure in the sheet (Japanese Patent Laid-Open Nos. 60-242035, 61-195132, 61-195133 and, 63-39602, USP 4,873,034, etc.). In another method of producing a microporous polyolefin membrane from a highly concentrated solution of UHMW polyolefin, the molecular weight distribution of a polyolefin composition containing UHMW is controlled within a specific range (USP 5,051,183). Although the microporous polyolefin membrane known in the art has a small pore size, it does not meet the requirement of the above secondary battery to have a high holding capacity and a high output level.

The lithium battery generates an intense heat due to short-circuit of the electrodes to cause ignition of lithium. Therefore, the battery separator should have a function to shut down the electric current flow through the separator membrane by clogging the pores, before lithium catches fire, with molten material which constitutes the membrane. However, since the known microporous polyolefin membranes are molten at a higher temperature, the pores are not effectively clogged at a temperature sufficiently low to prevent the ignition of lithium. Considering the above problems, it is desirable to lower the shutdown temperature to assure the safety of using the lithium battery. Thus, the lower the shutdown temperature and the larger the temperature difference between the shutdown temperature and the breakdown temperature of the membrane, the better the battery is in its safety and reliability.

Japanese Patent Application No. 60-23954 discloses a technique to provide a battery separator with the shutdown function at short circuit. This document teaches that the use of a single-layered microporous film of polypropylene or polyethylene is desirable to prevent the ignition or explosion of the battery due to the meltdown of the separator material being caused when the temperature in the battery is elevated by Joule's heat generated in the external short circuit. When a battery is externally shortcircuited, the temperature of the battery rises by Joule's heat to reach a melting point of the separator material, at which the single-layered microporous film of polypropylene or polyethylene begins to melt. The melt of separator material clogs the pores in the separator to prevent the ions from being transported through the separator, and makes the separator electrically insulating to shut off the current flow. Therefore, the temperature rise stops, and the ignition or explosion of the battery can be prevented.

However, at an elevated temperature around the melting point of a thermoplastic resin such as polyolefin, the cohesive force in the separator is so reduced that a separator comprising a single-layered microporous membrane is likely to be broken. Therefore, the problem of the ignition or explosion of battery still remains unsolved.

Accordingly, an object of the present invention is to provide a microporous membrane having a low shutdown temperature and a high meltdown temperature (high breakdown temperature) as well as having good permeability and

mechanical strength.

Another object of the present invention is to provide a microporous membrane having a large pore opening at the surface thereof so as to reduce the contact area between the microporous membrane and the surface of electrodes although having a small pore size inside the membrane.

Still another object of the present invention is to provide a microporous membrane having an enhanced holding capacity and a uniform surface appearance when wound on a winding tube so as to increase the capacity of a battery.

Yet another object of the present invention is to provide a microporous membrane having a reasonable thickness for safety.

As a result of the intense research in view of the above objects, the inventors have found that a composite membrane having the above properties can be obtained by laminating a specific microporous polyolefin membrane with at least one polyolefin nonwoven fabric having specific properties. The present invention has been accomplished via this finding.

Thus, in a first aspect of the present invention, there is provided a microporous polyolefin composite membrane comprising a microporous polyolefin membrane and a polyolefin nonwoven fabric laminated on at least one surface of the microporous polyolefin membrane, which composite membrane has a thickness of 25 to 200  $\mu\text{m}$ , a porosity of 30 to 70%, an air permeability of 100 to 2000 sec/100cc and a surface opening area ratio of 50 to 90% on at least one outer surface thereof, the microporous polyolefin membrane comprising a matrix polyolefin component which is a polyolefin having a weight average molecular weight of  $5 \times 10^5$  or more or a polyolefin mixture containing the polyolefin having a weight average molecular weight of  $5 \times 10^5$  or more, and having a porosity of 30 to 95%, an air permeability of 100 to 2000 sec/100cc, an average open pore diameter of 0.001 to 1  $\mu\text{m}$  and a tensile strength at break of 500 kg/cm<sup>2</sup> or more.

In a second aspect of the present invention, there is provided a battery separator comprising the microporous polyolefin composite membrane as specified above.

In a third aspect of the present invention, there is provided a method of producing the microporous polyolefin composite membrane as specified above, which comprises (1) preheating a starting polyolefin nonwoven fabric, (2) stacking the preheated polyolefin nonwoven fabric on at least one surface of a starting microporous polyolefin membrane without cooling the preheated polyolefin nonwoven fabric, and (3) calendering the stack.

#### [1] Microporous polyolefin membrane

The starting material for producing the microporous polyolefin membrane of the present invention having an open-celled structure mainly comprises a matrix polyolefin component and an optional shutdown polymer component. The matrix polyolefin component is a polyolefin having a weight average molecular weight (Mw) of  $5 \times 10^5$  or more or a polyolefin mixture containing thereof.

When Mw of the polyolefin is less than  $5 \times 10^5$ , an extruded gel sheet cannot be stretched at a sufficiently high stretch ratio, thereby failing to produce the microporous polyolefin membrane required in the present invention. The upper limit of Mw is not critical. However, a polyolefin having Mw exceeding  $15 \times 10^6$  may reduce the moldability in forming a gel sheet.

To prepare a highly concentrated polyolefin solution in the production process and to improve the mechanical strength of the resulting microporous polyolefin membrane, it is preferable to use as the matrix polyolefin component a polyolefin mixture containing a UHMW polyolefin having Mw of  $1 \times 10^6$  or more, preferably  $1 \times 10^6$  to  $15 \times 10^6$  and a high molecular weight (HMW) polyolefin having Mw of not less than  $1 \times 10^5$  and less than  $1 \times 10^6$ . The content of the UHMW polyolefin is 1 weight % or more, preferably 10 to 70 weight % based on the weight of the polyolefin mixture. The content of the HMW polyolefin is 99 weight % or less, preferably 30 to 90 weight % based on the weight of the polyolefin mixture. When the content of the UHMW polyolefin is less than 1 weight %, the entanglement of molecular chains contributing to the improvement of stretchability does not take place, failing to provide a high-strength microporous membrane.

The polyolefin for the matrix polyolefin component may be a crystalline homopolymer, a two-stage polymer, a copolymer or a blend thereof, each being obtained by polymerizing ethylene, propylene, 1-butene, 4-methyl-pentene-1, 1-hexene, etc. Among such polymers, polypropylene, polyethylene (particularly a high density polyethylene), and a mixture containing these polymers are preferable.

The ratio of weight average molecular weight/number average molecular weight (Mw/Mn) of the polyolefin and the polyolefin mixture, which is a measure showing uniformity of the molecular weight distribution, is preferably 300 or less, more preferably 5 to 50. When Mw/Mn exceeds 300, lower molecular weight components tend to be cut when stretched, resulting in the decrease in the overall strength of the resulting membrane.

An optional shutdown polymer component, i.e., a polymer which readily melts at a low temperature, preferably 135°C or lower, to clog or shut down the pores, may be used in combination with the matrix polyolefin component. Such a shutdown polymer may be a low density polyethylene and a low molecular weight polyethylene. The low density

polyethylene may include a high-pressure branched low density polyethylene (LDPE) preferably having a density of about 0.91 to 0.93 g/cm<sup>3</sup> and a melt index (MI measured at 190°C under a load of 2.16 kgf) of 0.1 to 20 g/10 min, more preferably 0.5 to 10 g/10 min, and a low-pressure linear low density polyethylene (LLDPE) preferably having a density of 0.91 to 0.93 g/cm<sup>3</sup> and MI of 0.1 to 25 g/10 min, preferably 0.5 to 10 g/10 min. The low molecular weight polyethylene (LMWPE) is preferred to have Mw of 1000 to 4000 and a melting point of 80 to 130°C. The shutdown polymer such as LDPE, LLDPE and LMWPE may be used in an amount of 5 to 30 weight %, preferably 5 to 25 weight % based on the total weight of the shutdown polymer and the matrix polyolefin component. When the amount is less than 5 weight %, the shutdown effect at a low temperature is insufficient and the porosity is reduced, and an amount more than 30 weight % remarkably reduces the mechanical strength of the resulting microporous polyolefin membrane.

The method of producing the microporous polyolefin membrane according to the present invention will be explained below.

In general, a starting material comprising the matrix polyolefin component and the optional shutdown polymer component is subjected to the steps of: addition of an organic liquid or solid and an optional inorganic fine powder; melt-kneading; extrusion into the form of sheet, stretching and extraction. Preferably, the starting material is dissolved in a good solvent for the polyolefins in the starting material to prepare a solution, which is extruded from a die into the form of sheet. The sheet is gelated by cooling to form a gel sheet, which is then stretched at an elevated temperature and extracted to remove the solvent remaining in the stretched sheet.

In more detail, the solution of the starting material is prepared by dissolving the starting material in a solvent under heating. The solvent is not specifically limited so long as it dissolves the starting material. Examples of the solvents include aliphatic or alicyclic hydrocarbons such as nonane, decane, undecane, dodecane, liquid paraffin, etc., and fractions of mineral oils having boiling points substantially equal to those of these hydrocarbons. Nonvolatile solvents such as liquid paraffin are preferable to obtain the gel sheet having uniform solvent contents. Dissolution of the starting material under heating may be carried out under vigorous stirring or kneading in an extruder at a temperature at which the starting material is completely dissolved in the solvent, preferably at 140 to 250°C. The concentration of the solution is preferably 10 to 80 weight %, more preferably 10 to 50 weight %. When the concentration is less than 10 weight %, a large amount of a solvent has to be used, and swelling and neck-in are likely to take place at the exit of a die in the process of forming sheets. Accordingly, it is difficult to produce large sheets. It is preferable to add an antioxidant to the solution to protect the polyolefin from degradation by oxidation.

Next, a heated solution of the starting material is extruded through a die into the form of sheet. Usually a sheet die having a rectangular orifice is used, and an inflation die having an annular orifice, etc. may be also used. When the sheet die is used, a die gap is usually 0.1 to 5 mm, and an extrusion temperature of the die is 140 to 250°C.

The solution extruded through the die is formed into a gel sheet by being cooled to the gelation temperature or lower. As a method of cooling, direct contact with cooling air, cooling water and other cooling media, contact with a roll cooled by a coolant, etc. may be employed. The solution extruded through a die may be drawn at a drawdown ratio of 1-10, preferably 1-5 before or after cooling.

The gel sheet is then subjected to a uniaxial or biaxial stretching treatment to impart a uniaxial or biaxial orientation to the gel sheet at a predetermined stretch ratio at an elevated temperature by an ordinary method such as a tenter method, a roll method, an inflation method, a calendering method, or a combination thereof. Biaxial stretching is preferable. It may be carried out by stretching the sheet in the machine direction (longitudinal direction) and a transverse direction (direction perpendicular to the machine direction) simultaneously or successively, and simultaneous biaxial stretching is more preferable.

The stretching temperature may be equal to or lower than a temperature which is 10°C above the melting point of the starting material, preferably in the range from the crystal dispersion temperature to the crystal melting point. The stretch ratio varies depending on the original thickness of the gel sheet. The stretch ratio for the longitudinal or transverse uniaxial stretching operation is preferably two times or more, more preferably 3 to 30 times the original length. The stretch ratio for the biaxial stretching operation is preferably 10 times or more, more preferably 15 to 400 times the original area. When the stretch ratio in the biaxial stretching is less than 10 times the original area, the resulting microporous membrane does not acquire a high modulus and a high mechanical strength due to an insufficient orientation. On the other hand, a stretch ratio exceeding 400 times the original area requires complicated and additional control of the stretching operation.

The thus stretched sheet is subjected to a solvent-removing treatment. Solvents used for the solvent-removing treatment may be highly volatile solvents including hydrocarbons such as pentane, hexane, heptane, etc.; chlorinated hydrocarbons such as methylene chloride and carbon tetrachloride; fluorinated hydrocarbons such as trifluoroethane; and ethers such as diethyl ether and dioxane. These volatile solvents may be used alone or in combination, and may be selected according to the nonvolatile solvents used to dissolve the starting material. The solvent remaining in the stretched sheet is removed by extracting the sheet with the above volatile solvent and/or spraying the volatile solvent on the sheet.

The solvent-removing treatment is repeated until the content of the residual solvent in the stretched sheet is re-

duced to less than 1 weight %. The stretched sheet is then dried to remove the volatile solvent by heating, air-cooling, etc. The dried stretched sheet is preferred to be heat-set at a temperature between the crystal dispersion temperature and the melting point.

The microporous polyolefin membrane produced as mentioned above has a porosity of 30 to 95%, an average open pore diameter of 0.001 to 1  $\mu\text{m}$ , a tensile strength at break of 500 kg/cm<sup>2</sup> or more, an air permeability of 100 to 2000 sec/100cc, and a surface opening area ratio of 30 to 70 %. The thickness of the microporous polyolefin membrane is generally 5 to 50  $\mu\text{m}$  before being subjected to the subsequent laminating treatment.

The porosity of the microporous polyolefin membrane of the present invention may be defined as a percent ratio of the total volume occupied by the void space of a sample membrane to the bulk volume of the same sample which is the sum of the void space volume and the volume occupied by the solid material of the membrane, and calculated from the equation: % porosity = (1 - density of sample membrane/density of starting material) x 100.

The porosity of the microporous polyolefin membrane of the present invention is 30 to 95%, and preferably 30 to 50%. A porosity less than 30% is undesirable because the holding capacity of the membrane for the electrolyte solution is reduced, and a porosity more than 95% reduces the mechanical strength of the membrane to make the membrane scarcely fit for use.

The average open pore diameter referred to in the present invention is the average diameter of pores which are interconnected through more or less tortuous paths which extends from one exterior surface of the microporous polyolefin membrane to another. The average open pore diameter of the microporous polyolefin membrane of the present invention is 0.001 to 1  $\mu\text{m}$ , preferably 0.001 to 0.5  $\mu\text{m}$ , and more preferably 0.005 to 0.1  $\mu\text{m}$ . When the average open pore diameter is smaller than 0.001  $\mu\text{m}$ , the electrolyte solution cannot penetrate into the pores or cells, thereby making the ion transport through the open pores difficult. When the average open pore diameter exceeds 1  $\mu\text{m}$ , the diffusion of the electrode active materials and the reaction products cannot be prevented.

To enhance the mechanical strength and prevent the tearing of the membrane, the tensile strength at break, measured according to ASTM D882, of the microporous polyolefin membrane is 500 kg/cm<sup>2</sup> or more.

The surface opening area ratio in the present invention means an area ratio of the total area occupied by the void opening of the pores on the surface of the microporous polyolefin membrane to the total surface area of the microporous polyolefin membrane which is the sum of the void surface area and the surface area occupied by the solid material. The surface opening area ratio is 30 to 70%.

### 30 [2] Polyolefin nonwoven fabric

Micro fibers for the polyolefin nonwoven fabric to be laminated on the microporous polyolefin membrane are preferred to have diameters from 0.1 to 5  $\mu\text{m}$ . The basis weight of the polyolefin nonwoven fabric is preferably 5 to 50 g/m<sup>2</sup>, and more preferably 7 to 45 g/m<sup>2</sup>. The air permeability is preferably 0.1 to 100 sec/100 cc. The thickness before subjection to the lamination treatment is preferably 30 to 500  $\mu\text{m}$ .

The polyolefin nonwoven fabric may be produced from fibers of a crystalline homopolymer, a two-stage polymer, a copolymer or a blend thereof, each polymer being produced from ethylene, propylene, 1-butene, 4-methyl-pentene-1, 1-hexene, etc. Of the above polyolefin nonwoven fabrics, those produced by polypropylene fibers, polyethylene fibers, etc. are preferable. The polyolefin nonwoven fabric used in the present invention may be produced by a method known in the art.

### 45 [3] Microporous polyolefin composite membrane

The microporous polyolefin membrane described above is liable to change in its structure. However, when treated at an elevated temperature within a specific range during the lamination process, the surface of the microporous polyolefin membrane acquires a fine roughness which allows the microporous polyolefin membrane layer to strongly bond to the polyolefin nonwoven fabric layer without changing the properties of the microporous polyolefin membrane before being subjected to the lamination process. Therefore, the microporous polyolefin composite membrane of the present invention is produced by the lamination treatment of a stack of the microporous polyolefin membrane and the polyolefin nonwoven fabric under suitable heating.

A starting polyolefin nonwoven fabric having a thickness of 30 to 500  $\mu\text{m}$  is preheated and regulated in its thickness at 50 to 120°C, preferably 50 to 100°C for 2 to 60 seconds with or without applying a compression pressure of about 5 to 30 kgf/cm<sup>2</sup> by passing the starting polyolefin nonwoven fabric through a pair of heating pressure rolls, etc. When the preheating temperature is lower than 50°C, the preheating is insufficient, and the surface opening area ratio is reduced when the preheating temperature is higher than 120°C.

Separately, a starting microporous polyolefin membrane may be optionally preheated, if desired, at 50 to 100°C for 2 to 60 seconds.

The polyolefin nonwoven fabric thus preheated and the microporous polyolefin membrane optionally preheated

are stacked each other immediately after each preheating, and calendered at 50 to 140°C, preferably 90 to 120°C while applying a compression pressure of 5 to 30 kgf/cm<sup>2</sup>, preferably 5 to 20 kgf/cm<sup>2</sup> by passing the stack through a plurality of pairs of the calender rolls to obtain a microporous polyolefin composite membrane of the present invention. If the calender roll pressure is less than 5 kgf/cm<sup>2</sup>, the bonding strength between the microporous polyolefin membrane and the polyolefin nonwoven fabric is insufficient, and the surface opening area ratio of the polyolefin nonwoven fabric is reduced when exceeding 30 kgf/cm<sup>2</sup>. When the calendering temperature exceeds 140°C, the permeability of the microporous polyolefin membrane is reduced, whereas the bonding of the microporous polyolefin membrane and the polyolefin nonwoven fabric is insufficient when the calendering temperature is lower than 50°C.

The polyolefin nonwoven fabric may be laminated on one of the surfaces of the microporous polyolefin membrane or may be laminated on both the surfaces of the microporous polyolefin membrane. Thus, the preferred layered structure of the microporous polyolefin composite membrane of the present invention is a two-layered structure of microporous polyolefin membrane/polyolefin nonwoven fabric and a three-layered structure of polyolefin nonwoven fabric/microporous polyolefin membrane/polyolefin nonwoven fabric.

The total thickness of the microporous polyolefin composite membrane thus produced is preferably 25 to 200 µm, and more preferably 25 to 100 µm.

The microporous polyolefin composite membrane of the present invention has a surface opening area ratio of 50 to 90% on at least one outer surface thereof. When the surface opening area ratio is less than 50%, a sufficient effective surface area of the electrodes cannot be ensured, and the capacity and electric characteristics of battery cannot be improved because the holding capacity of the separator for the electrolyte solution is not increased. In addition, the by-product is not effectively captured by the separator. On the other hand, when the surface opening area ratio is larger than 90%, the mechanical strength of the microporous polyolefin composite membrane (separator) is poor.

The porosity of the microporous polyolefin composite membrane is 30 to 70%, preferably 30 to 50%, and the air permeability is 100 to 2000 sec/100cc, preferably 200 to 1500 sec/100cc.

The microporous polyolefin composite membrane of the present invention further has a shutdown temperature, at which the air permeability of the composite membrane is raised to 100,000 sec/100 cc or more, which is preferably 135°C or lower, more preferably 105 to 135°C, and a meltdown temperature at which the separator (microporous polyolefin composite membrane) is broken or ruptured due to the meltdown of the matrix polyolefin which is preferably 165°C or higher.

Also, the holding capacity for the electrolyte solution of the microporous polyolefin composite membrane, which is represented by a weight percent ratio of the amount of γ-butyrolactone held in the microporous polyolefin composite membrane to the weight of the microporous polyolefin composite membrane, is preferably 30 to 80%, preferably 35 to 80%.

The present invention will be further described while referring to the following Examples which illustrate various preferred embodiments of the present invention.

In the following examples and comparative examples, each property was measured as follows.

(1) Thickness

Measured by observing the cross section under a scanning electron microscope.

(2) Air permeability

Measured according to JIS P8117.

(3) Porosity

Determined by measuring the density of the starting material and the density of the membrane, and calculating the equation: (1 - density of sample membrane/density of starting material) × 100.

(4) Average open pore diameter

Determined by using Omnisorp 360 manufactured by Nikkiso KK

(5) Surface opening area ratio and opening pore size

Determined from electron microphotograph.

(6) Tensile strength at break

Measured according to ASTM D882 using a rectangular sample having a width of 10 mm.

(7) Shutdown temperature

The temperature at which the air permeability reached 100,000 sec/100cc or more was measured by heating the sample composite membrane.

(8) Meltdown temperature

The temperature at which the sample composite membrane was broken due to meltdown of the matrix polyolefin was measured by heating the sample composite membrane.

(9) Holding capacity

The weight of γ-butyrolactone held in the sample composite membrane was measured, and the holding capacity was represented by the ratio of the weight of γ-butyrolactone to the weight of the sample composite mem-

brane.

(10) Sagging amount

The surface appearance of as-wound membrane was evaluated by the amount of sagging. A rectangular sample (1.5 m length and 0.4 m width) of the composite membrane was horizontally supported on a pair of rolls spaced 1 m apart (between the centers) while one of the ends of the sample was fixed. A load of 0.4 kgf was put on the other end equally and gravitationally, and the sagging amount of the central portion of the sample composite membrane was measured. The maximum value after several repeated measurements was employed. When a membrane having a large sagging amount is wound on a winding tube, the surface of as-wound membrane presents a wavy appearance.

10

EXAMPLE 1

A polyolefin mixture consisting of 6 parts by weight of a UHMW polyethylene having Mw of  $2.5 \times 10^6$  and 24 parts by weight of an HMW polyethylene (high density polyethylene) having Mw of  $3.5 \times 10^5$  was prepared. To 100 parts by weight of the polyolefin mixture thus prepared, were added 0.375 parts by weight of an antioxidant. The 30 parts by weight of the resultant mixture was fed into a twin screw intensive extruder (outer diameter = 58 mm, and L/D = 42). The mixture was melt-kneaded in the extruder while feeding 70 parts by weight of a liquid paraffin from a side feeder to prepare a polyolefin solution.

The polyolefin solution was extruded from a T-die of the extruder into the form of sheet which was taken-up by a pair of cooling rolls to form a gel sheet. The gel sheet was subjected to a simultaneous biaxial stretching by a stretch ratio of 5 times the original length in both the machine direction and the transverse direction at 115°C to obtain a stretched membrane, which was then washed by methylene chloride to remove the liquid paraffin remaining in the membrane, dried and heat-set at 120°C to produce a microporous polyethylene membrane of a thickness of 25 µm.

The microporous polyethylene membrane thus produced was laminated with a melt-blown polypropylene nonwoven fabric (fiber diameter: 4 µm; basis weight: 7 g/m<sup>2</sup>; thickness: 60 µm) by calendering under the conditions shown in Table 1 to obtain a microporous polyethylene composite membrane.

EXAMPLE 2

Except for using a polyolefin mixture consisting of 6 parts by weight of the same UHMW polyethylene, 24 parts by weight of the same HMW polyethylene and 5 parts by weight of LDPE (density: 0.91 g/cm<sup>3</sup>; MI: 2.0 g/10 min), and regulating the thickness of the microporous polyethylene membrane to 15 µm, the same procedures as in Example 1 were repeated to obtain a microporous polyethylene composite membrane.

EXAMPLE 3

Except for using a polyolefin mixture consisting of 6 parts by weight of the same UHMW polyethylene, 24 parts by weight of the same HMW polyethylene and 5 parts by weight of LMWPE (melting point: 126°C; Mw: 4000), and regulating the thickness of the microporous polyethylene membrane to 15 µm, the same procedures as in Example 1 were repeated to obtain a microporous polyethylene composite membrane.

EXAMPLE 4

Except for using a polyolefin mixture consisting of 6 parts by weight of the same UHMW polyethylene, 24 parts by weight of the same HMW polyethylene and 5 parts by weight of LMWPE (melting point: 116°C; Mw: 1000), and regulating the thickness of the microporous polyethylene membrane to 15 µm, the same procedures as in Example 1 were repeated to obtain a microporous polyethylene composite membrane.

EXAMPLE 5

Except for laminating the polypropylene nonwoven fabrics on both the surface of the microporous polyethylene membrane, the same procedures as in Example 1 were repeated to obtain a microporous polyethylene composite membrane of three-layered structure.

EXAMPLE 6

Except for using a polypropylene nonwoven fabric (fiber diameter: 4 µm; basis weight: 40 g/m<sup>2</sup>; thickness: 440 µm), the same procedures as in Example 1 were repeated to obtain a microporous polyethylene composite membrane.

## EXAMPLE 7

Except for using a polypropylene nonwoven fabric (fiber diameter: 4 µm; basis weight: 22 g/m<sup>2</sup>; thickness: 230 µm) and changing the calendering temperature to 120°C, the same procedures as in Example 1 were repeated to obtain a microporous polyethylene composite membrane.

## COMPARATIVE EXAMPLE 1

The microporous polyethylene membrane of Example 1 having no laminated polyolefin nonwoven fabric was used.

The properties of the above microporous polyethylene composite membranes (Examples 1 to 7) and the microporous polyolefin membrane (Comparative Example 1), measured as described above, are shown in Table 1.

Table 1 (to be contd.)

	<u>Examples</u>			
	1	2	3	4
<b>MICROPOROUS POLYOLEFIN MEMBRANE</b>				
Composition (parts by weight)				
UHMWPE	6	6	6	6
HDPE	24	24	24	24
LDPE	-	5	-	-
LMWPE	-	-	5	5

35

40

45

50

Thickness ( $\mu\text{m}$ )	25	15	15	15
Air permeability (sec/100cc)	590	250	250	250
Porosity (%)	40	37	38	35
Average open pore diameter ( $\mu\text{m}$ )	0.030	0.025	0.025	0.025
Surface opening area ratio (%)	40	40	40	40
Tensile strength at break ( $\text{kg/cm}^2$ )				
MD	1225	1160	1063	965
TD	944	830	912	740
<b>POLYOLEFIN NONWOVEN FABRIC</b>				
Polyolefin	PP	PP	PP	PP
Thickness ( $\mu\text{m}$ )	60	60	60	60
Basis weight ( $\text{g/m}^2$ )	7	7	7	7
Air permeability (sec/100cc)	<1	<1	<1	<1
<b>PRODUCTION CONDITIONS</b>				
Preheating temperature of polyolefin nonwoven fabric ( $^\circ\text{C}$ )	80	80	80	80
Calendering temperature ( $^\circ\text{C}$ )	115	115	115	115
Calendering pressure ( $\text{kgf/cm}^2$ )	10	10	10	10
Calendering speed (m/min)	7	7	7	7
<b>COMPOSITE MEMBRANE</b>				
Number of layers	2	2	2	2
Thickness ( $\mu\text{m}$ )	40	30	32	31
Porosity (%)	45	50	50	50
Air permeability (sec/100cc)	592	712	632	720
Shutdown temperature ( $^\circ\text{C}$ )	135	125	115	105
Meltdown temperature ( $^\circ\text{C}$ )	185	185	185	185
Surface opening area ratio (%)				
observe	75	75	75	75
reverse	40	37	38	35
Surface pore size ( $\mu\text{m}$ )				
observe	20	20	20	20
reverse	0.03	0.03	0.03	0.03
Holding capacity (wt. %)	61	67	68	66
Sagging amount (mm)	3	4	5	5

Table 1 (contd.)

	<u>Examples</u>			<u>Com. Ex.</u>
	5	6	7	1
<b>MICROPOROUS POLYOLEFIN MEMBRANE</b>				
Composition (parts by weight)				
UHMWPE	6	6	6	6
HDPE	24	24	24	24
LDPE	-	-	-	-
LMWPE	-	-	-	-
Thickness ( $\mu\text{m}$ )	25	25	25	25
Air permeability (sec/100cc)	590	590	590	590
Porosity (%)	40	40	40	40
Average pore diameter ( $\mu\text{m}$ )	0.030	0.030	0.030	0.030
Surface opening area ratio (%)	40	40	40	40
Tensile strength at break ( $\text{kg/cm}^2$ )				
MD	1225	1225	1225	1225
TD	944	944	944	944
<b>POLYOLEFIN NONWOVEN FABRIC</b>				
Polyolefin	PP	PP	PP	-
Thickness ( $\mu\text{m}$ )	60	440	230	-
Basis weight ( $\text{g/m}^2$ )	7	40	22	-
Air permeability (sec/100cc)	<1	<1	<1	-
<b>PRODUCTION CONDITIONS</b>				
Preheating temperature of polyolefin nonwoven fabric ( $^\circ\text{C}$ )	80	80	80	-
Calendering temperature ( $^\circ\text{C}$ )	115	115	120	-
Calendering pressure ( $\text{kgt/cm}^2$ )	10	10	10	-
Calendering speed (m/min)	7	7	7	-
<b>COMPOSITE MEMBRANE</b>				
Number of layers	3	2	2	1
Thickness ( $\mu\text{m}$ )	64	135	100	25
Porosity (%)	43	70	60	40

Air permeability (sec/100cc)	722	960	958	612
Shutdown temperature (°C)	135	135	135	135
Meltdown temperature (°C)	185	185	185	165
Surface opening area ratio (%)				
observe	76	68	70	40
reverse	77	40	40	40
Surface pore size (μm)				
observe	20	17	18	0.03
reverse	20	0.03	0.03	0.03
Holding capacity (wt. %)	58	72	70	39
Sagging amount (mm)	3	3	3	15

## EXAMPLE 8

A microporous polyethylene membrane produced in the same manner as in Example 1 was laminated with a polypropylene nonwoven fabric (fiber diameter: 4 μm; basis weight: 7 g/m<sup>2</sup>; thickness: 50 μm; air permeability: less than 1 sec/100cc) by calendering under the conditions shown in Table 2 to obtain a microporous polyethylene composite membrane.

## EXAMPLE 9

Except for changing the calendering temperature and the calendering pressure to 100°C and 10 kgf/cm<sup>2</sup>, the same procedures as in Example 8 were repeated to obtain a microporous polyethylene composite membrane.

## EXAMPLE 10

Except for laminating a microporous polyethylene membrane having a thickness of 15 μm and an air permeability of 200 sec/100cc with a polypropylene nonwoven fabric (fiber diameter: 4 μm; basis weight: 6 g/m<sup>2</sup>; thickness: 30 μm; air permeability: less than 1 sec/100cc), the same procedures as in Example 8 were repeated to obtain a microporous polyethylene composite membrane.

## EXAMPLE 11

Except for laminating two sheets of polypropylene nonwoven fabrics (fiber diameter: 4 μm; basis weight: 6 g/m<sup>2</sup>; thickness: 30 μm; air permeability: less than 1 sec/100cc) on both the surface of a microporous polyethylene membrane having a thickness of 15 μm and an air permeability of 200 sec/100cc and changing the calendering temperature to 115°C, the same procedures as in Example 8 were repeated to obtain a microporous polyethylene composite membrane of three-layered structure.

## EXAMPLE 12

Except for laminating a microporous polyethylene membrane having an air permeability of 560 sec/100cc with a polyethylene nonwoven fabric (Tyvek® manufactured by E. I. Du Pont de Nemours and Company; thickness: 100 μm; basis weight: 41 g/m<sup>2</sup>; air permeability: 100 sec/100cc) and changing the calendering pressure and the calendering speed to 5 kg/cm<sup>2</sup> and 3 m/min, the same procedures as in Example 8 were carried out to obtain a microporous polyethylene composite membrane.

## EXAMPLE 13

Except for changing the calendering temperature to 105°C, the same procedures as in Example 12 were carried out to obtain a microporous polyethylene composite membrane.

## COMPARATIVE EXAMPLE 2

The microporous polyethylene membrane of Example 8 having no laminated polyolefin nonwoven fabric was used.

## 5 COMPARATIVE EXAMPLE 3

Except for changing the calendering temperature to 145°C, the same procedures as in Example 8 were repeated to obtain a microporous polyethylene composite membrane.

## 10 COMPARATIVE EXAMPLE 4

Except for using a microporous polyethylene membrane having an air permeability of 2119 sec/100cc, porosity of 27% and average pore size of 0.020 µm, the same procedures as in Example 8 were repeated to obtain a microporous polyethylene composite membrane.

## 15 COMPARATIVE EXAMPLE 5

Except for using a polypropylene nonwoven fabric (fiber diameter: 4 µm; basis weight: 55 g/m<sup>2</sup>; thickness: 100 µm) and changing the calendering temperature to 120°C, the same procedures as in Example 8 were repeated. However, both the polypropylene nonwoven fabric and the microporous polyethylene membrane were not bonded to each other thus failing to obtain a microporous polyethylene composite membrane.

The properties of the above microporous polyethylene composite membranes (Examples 8 to 13 and Comparative Examples 3 and 4) and the microporous polyolefin membrane (Comparative Example 2), measured as described above, are shown in Table 2.

## 25

Table 2 (to be contd.)

	Examples				
	8	9	10	11	12
<b>MICROPOROUS POLYOLEFIN MEMBRANE</b>					
Composition (parts by weight)					
UHMWPE	6	6	6	6	6
HDPE	24	24	24	24	24
40 LDPE	-	-	-	-	-
LMWPE	-	-	-	-	-
Thickness (µm)	25	25	15	15	25
45 Air permeability (sec/100cc)	590	590	200	200	560
Porosity (%)	40	40	40	40	40

50

55

## EP 0 811 479 A2

Average pore diameter ( $\mu\text{m}$ )	0.030	0.030	0.030	0.030	0.030
Surface opening area ratio (%)	40	40	40	40	40
Tensile strength at break ( $\text{kg/cm}^2$ )					

MD	1225	1225	1200	1200	1225
TD	945	945	920	920	945

## POLYOLEFIN NONWOVEN FABRIC

Polyolefin	PP	PP	PP	PP	PE
Thickness ( $\mu\text{m}$ )	50	50	30	30	100
Basis weight ( $\text{g/m}^2$ )	7	7	6	6	41
Air permeability (sec/100cc)	<1	<1	<1	<1	100

## PRODUCTION CONDITIONS

Preheating temperature of polyolefin nonwoven fabric ( $^\circ\text{C}$ )	80	80	80	80	80
Calendering temperature ( $^\circ\text{C}$ )	110	100	110	115	110
Calendering pressure ( $\text{kgt/cm}^2$ )	16	10	16	16	5
Calendering speed (m/min)	20	20	20	20	3

## COMPOSITE MEMBRANE

Number of layers	2	2	2	3	2
Thickness ( $\mu\text{m}$ )	45	50	32	72	122
Porosity (%)	45	45	46	42	40
Air permeability (sec/100cc)	630	612	252	956	1010
Shutdown temperature ( $^\circ\text{C}$ )	135	135	135	135	120
Meltdown temperature ( $^\circ\text{C}$ )	185	185	185	185	165
Surface opening area ratio (%)					
observe reverse	76 40	79 40	72 40	76 77	59 40
Surface pore size ( $\mu\text{m}$ )					
observe reverse	20 0.03	20 0.03	18 0.03	20 20	30 0.03
Holding capacity (wt. %)	57.6	59.4	61.3	58.0	55.5
Sagging amount (mm)	4	3	3	2	5

Table 2 (contd.)

	Example	Comparative Examples				
		13	2	3	4	
<b>MICROPOROUS POLYOLEFIN MEMBRANE</b>						
Composition (parts by weight)						
UHMWPE	6	6	6	6	6	
HDPE	24	24	24	24	24	
LDPE	-	-	-	-	-	
LMWPE	-	-	-	-	-	
Thickness ( $\mu\text{m}$ )	25	25	25	25	25	
Air permeability (sec/100cc)	560	590	590	2119	590	
Porosity (%)	40	40	40	27	40	
Average pore diameter ( $\mu\text{m}$ )	0.030	0.030	0.030	0.020	0.030	
Surface opening area ratio (%)	40	40	40	25	40	
Tensile strength at break ( $\text{kg/cm}^2$ )						
MD	1225	1225	1225	1415	1225	
TD	945	945	945	1100	945	
<b>POLYOLEFIN NONWOVEN FABRIC</b>						
Polyolefin	PE	-	PP	PP	PP	
Thickness ( $\mu\text{m}$ )	100	-	50	50	100	
Basis weight ( $\text{g/m}^2$ )	41	-	7	7	55	
Air permeability (sec/100cc)	100	-	<1	<1	<1	
<b>PRODUCTION CONDITIONS</b>						
Preheating temperature of polyolefin nonwoven fabric ( $^\circ\text{C}$ )	80	-	80	80	80	
Calendering temperature ( $^\circ\text{C}$ )	105	-	145	110	120	
Calendering pressure ( $\text{kgt/cm}^2$ )	5	-	16	16	16	
Calendering speed (m/min)	3	-	20	20	20	
<b>COMPOSITE MEMBRANE</b>						
Number of layers	2	1	2	2	-	
Thickness ( $\mu\text{m}$ )	125	25	45	45	-	
Porosity (%)	40	37	45	40	-	

Air permeability (sec/100cc)	962	590	3219	2427	-
Shutdown temperature (°C)	120	135	135	135	-
Meltdown temperature (°C)	165	165	185	185	-
Surface opening area ratio (%)					
observe	60	40	76	76	-
reverse	40	40	32	23	-
Surface pore size (μm)					
observe	30	0.03	20	20	-
reverse	0.03	0.03	0.03	0.02	-
Holding capacity (wt. %)	56.3	38.5	61	50	-
Sagging amount (mm)	5	15	4	5	-

As seen from the results, the microporous polyolefin composite membranes of the present invention are well-balanced in the properties required for a battery separator. Namely, they have a low shutdown temperature, a high meltdown temperature, a high air permeability, a large opening area of the surface pores, a small size of the inside pores, a large holding capacity for the electrolyte solution, etc. In addition, since the microporous polyolefin membrane and the polyolefin nonwoven fabric are laminated at a relatively low temperature without using any adhesive, the electrolytes in the solution are effectively transported through the microporous polyolefin composite membrane without being hindered at the interface between the microporous polyolefin membrane and the polyolefin nonwoven fabric. Therefore, the microporous polyolefin composite membranes of the present invention are useful as battery separators.

### Claims

1. A microporous polyolefin composite membrane comprising a microporous polyolefin membrane and a polyolefin nonwoven fabric laminated on at least one surface of said microporous polyolefin membrane, which composite membrane has a thickness of 25 to 200 μm, a porosity of 30 to 70%, an air permeability of 100 to 2000 sec/100cc and a surface opening area ratio of 50 to 90% on at least one outer surface thereof, said microporous polyolefin membrane comprising a matrix polyolefin component which is a polyolefin having a weight average molecular weight of  $5 \times 10^5$  or more or a polyolefin mixture containing said polyolefin having a weight average molecular weight of  $5 \times 10^5$  or more and having a porosity of 30 to 95%, an air permeability of 100 to 2000 sec/100cc, an average open pore diameter of 0.001 to 1 μm and a tensile strength at break of 500 kg/cm<sup>2</sup> or more.
2. A microporous polyolefin composite membrane as claimed in claim 1, wherein said polyolefin nonwoven fabric comprises fine fibers having a diameter of 0.1 to 50 μm, and has an air permeability of 0.1 to 100 sec/100cc and a basis weight of 5 to 50 g/m<sup>2</sup>.
3. A microporous polyolefin composite membrane as claimed in claim 1 or 2, wherein said polyolefin mixture comprises an ultrahigh molecular weight polyolefin having a weight average molecular weight of  $1 \times 10^6$  to  $15 \times 10^6$  and a high molecular weight polyolefin having a weight average molecular weight of  $1 \times 10^5$  or more and less than  $1 \times 10^6$ .
4. A microporous polyolefin composite membrane as claimed in any one of claims 1 to 3, wherein said microporous polyolefin membrane comprises 70 to 95 weight % of said matrix polyolefin component and 5 to 30 weight % of a shutdown polymer component selected from the group consisting of a low molecular weight polyethylene, a low density polyethylene and a linear low density polyethylene, each weight percentage being based on the total weight of said matrix polyolefin component and said shutdown polymer component.
5. A microporous polyolefin composite membrane as claimed in any one of claims 1 to 4, wherein said low molecular weight polyethylene has a weight average molecular weight of 1000 to 4000 and a melting point of 80 to 130°C.

6. A microporous polyolefin composite membrane as claimed in any one of claims 1 to 5, wherein said low density polyethylene has a density of 0.91 to 0.93 g/cm<sup>3</sup> and a melt flow index of 0.1 to 20 g/10 min when measured at 190°C under a load of 2.16 kgf.

5 7. A microporous polyolefin composite membrane as claimed in any one of claims 1 to 6, wherein said linear low density polyethylene has a density of 0.91 to 0.93 g/cm<sup>3</sup> and a melt flow index of 0.1 to 25 g/10 min when measured at 190°C under a load of 2.16 kgf.

10 8. A microporous polyolefin composite membrane as claimed in any one of claims 1 to 7, having a shutdown temperature of 135°C or lower.

9. A microporous polyolefin composite membrane as claimed in any one of claims 1 to 8, having a meltdown temperature of 165°C or higher.

15 10. A battery separator comprising a microporous polyolefin composite membrane as defined in any one of claims 1 to 9.

11. A method for producing a microporous polyolefin composite membrane as defined in any one of claims 1 to 9, comprising:  
20 - preheating a starting polyolefin nonwoven fabric comprising fine fibers having a diameter of 0.1 to 50 µm, and having a thickness of 30 to 500 µm, an air permeability of 0.1 to 100 sec/100cc and a basis weight of 5 to 50 g/m<sup>2</sup> at 50 to 120°C;  
25 stacking, without cooling, said preheated polyolefin nonwoven fabric on at least one surface of a starting microporous polyolefin membrane comprising a matrix polyolefin component which is a polyolefin having a weight average molecular weight of 5 x 10<sup>5</sup> or more or a polyolefin mixture containing said polyolefin having a weight average molecular weight of 5 x 10<sup>5</sup> or more and having a thickness of 5 to 50 µm, a porosity of 30 to 95%, an air permeability of 100 to 2000 sec/100cc, an average open pore diameter of 0.001 to 1 µm and a tensile strength at break of 500 kg/cm<sup>2</sup> or more; and  
30 calendering the stack at 50 to 140°C under a pressure of 5 to 30 kgf/cm<sup>2</sup>.

35

40

45

50

55



(19) Europäisches Patentamt  
European Patent Office  
Office européen des brevets



(11) EP 0 811 479 A3

(12) EUROPEAN PATENT APPLICATION

(88) Date of publication A3:  
09.09.1998 Bulletin 1998/37

(51) Int Cl. 6: B32B 5/24, B32B 27/32,  
D04H 13/00, H01M 2/16

(43) Date of publication A2:  
10.12.1997 Bulletin 1997/50

(21) Application number: 97303786.4

(22) Date of filing: 03.06.1997

(84) Designated Contracting States:  
AT BE CH DE DK ES FI FR GB GR IE IT LI LU MC  
NL PT SE

Designated Extension States:  
AL LT LV RO SI

(30) Priority: 04.06.1996 JP 163776/96  
02.08.1996 JP 220465/96

(71) Applicant: Tonen Chemical Corporation  
Tokyo (JP)

(72) Inventors:  
• Takita, Kotaro, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)

- Kono, Koichi, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)
- Kaimai, Norimitsu, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)
- Yamaguchi, Soichiro, c/o Tonen Chem. Corp.  
Kawasaki-ku, Kawasaki-shi, Kanagawa-ken (JP)

(74) Representative: Calamita, Roberto  
Frank B. Dehn & Co.,  
European Patent Attorneys,  
179 Queen Victoria Street  
London EC4V 4EL (GB)

(54) **Microporous polyolefin composition membrane, production method thereof and battery separator**

(57) A microporous polyolefin composite membrane, preferably for use as a battery separator, comprising a microporous polyolefin membrane and a polyolefin nonwoven fabric laminated on at least one surface of the microporous polyolefin membrane. The composite membrane has a thickness of 25 to 200 µm, a porosity of 30 to 70%, an air permeability of 100 to 2000 sec/100cc and a surface opening area ratio of 50 to 90% on at least one outer surface thereof. The microporous polyolefin membrane comprises a matrix polyolefin component which is a polyolefin having a weight average molecular weight of  $5 \times 10^5$  or more or a polyolefin mixture containing the polyolefin having a weight aver-

age molecular weight of  $5 \times 10^5$  or more, and has a porosity of 30 to 95%, an air permeability of 100 to 2000 sec/100cc, an average open pore diameter of 0.001 to 1 µm and a tensile strength at break of 500 kg/cm<sup>2</sup> or more. The microporous polyolefin membrane may further comprise a shutdown polymer component to shut down the pores, thereby making the composite membrane impermeable. The polyolefin nonwoven fabric comprises fine fibers and has an air permeability of 0.1 to 100 sec/100cc and a basis weight of 5 to 50 g/m<sup>2</sup>. The polyolefin nonwoven fabric prevents the composite membrane from melting down at a low temperature thereby preventing the short-circuit between the electrodes.



European Patent  
Office

## EUROPEAN SEARCH REPORT

Application Number

EP 97 30 3786

DOCUMENTS CONSIDERED TO BE RELEVANT			CLASSIFICATION OF THE APPLICATION (Int.Cl.6)	
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.6)	
X	EP 0 355 214 A (TOA NENRYO KOGYO KK) 28 February 1990	1,10	B32B5/24 B32B27/32	
Y	* page 3, line 18-23 - page 4, line 13-55-58; claims 1,9,10; table 1 * * page 5, line 8 *	11	D04H13/00 H01M2/16 C08L23/06 B23B5/26	
X	EP 0 476 198 A (TONEN CORP) 25 March 1992	1,3,10	H01M2/14	
Y	* page 3, line 29-34 - page 4, line 9-37-48; claims 1,2,10 *	11	C08J5/22	
X	DATABASE WPI Section Ch, Week 9438 Derwent Publications Ltd., London, GB; Class A32, AN 94-307404 XP002072018 & JP 06 234 181 A (MITSUBISHI KASEI CORP) * abstract *	1,10	---	
A	DATABASE WPI Section Ch, Week 9603 Derwent Publications Ltd., London, GB; Class A85, AN 96-027629 XP002072019 & JP 07 302 584 A (DAICEL CHEM IND LTD) * abstract *	---	TECHNICAL FIELDS SEARCHED (Int.Cl.6)	
A	DATABASE WPI Section Ch, Week 9516 Derwent Publications Ltd., London, GB; Class A23, AN 95-118368 XP002072020 & JP 07 040 485 A (UNITIKA LTD) * abstract *	---	D04H C08L B23B H01M C08J	
The present search report has been drawn up for all claims				
Place of search	Date of completion of the search	Examiner		
THE HAGUE	21 July 1998	Derz, T		
CATEGORY OF CITED DOCUMENTS				
X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document				
T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document				